

## Temperature regime in neutron production target for BNCT

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*One of the problems in creation of the neutron production target for BNCT consists in necessity to spread the proton beam about the whole target surface to avoid the local overheating, caused by inhomogeneous distribution of energy deposition. Defocusing of the beam up to the target size creates some technical complications. More attractive looks the target moving across the beam, or the beam sweeping across the target.*

Temperature of target heating, caused by the energy deposition under a particle beam passing through, is defined by the thermal conductivity equation  $\frac{\partial T}{\partial t} = a^2 \Delta T + \frac{q(x, y, z, t)}{C_p}$  (1) with proper boundary conditions, one of which is that of practically no heat evacuation from the inlet target surface, i.e.  $\frac{\partial T}{\partial z} = 0$  at  $z=0$ . Function  $q(x, y, z, t)$  in (1) describes the specific power deposition in dependence on coordinates and time.

In case of a permanent particle beam the temperature in target is growing until the equilibrium is achieved between the power deposition and evacuation. The temperature stabilization time  $\tau_\infty$  is important to be known to make estimations on efficiency of moving target. When  $\tau_\infty$  is small compared to a time of material exposure under the beam,  $\tau_b \cong 2x_0 / u_0$  with  $2x_0$  standing for the beam size in the motion direction and  $u_0$  - for velocity, the target motion gives practically no effect. If, by the opposite,  $\tau_\infty$  is much more than  $\tau_b$ , only the last defines the maximum temperature.

To solve the equation (1) the operational method of complex variable function theory is convenient to be used. Time dependence of specific power deposition has a form  $q(x, y, z, t) = q_0(x, y, z) \cdot \eta(t)$ , where  $\eta(t)$  is the unit function, equal to zero when  $t < 0$ , and to unity when  $t \geq 0$ , whose image is  $1/p$ .

If the transverse size of the beam is much more than the target depth, the dependence of energy deposition on transverse coordinates may be neglected, so that  $q_0(x, y, z) \cong q_0(z)$ . Besides this  $q_0(z)$  may be considered equal to a constant value  $q_{00}$  within the mean range of particles  $\delta \cong 15 \mu m$ , and to zero outside it. Thus the temperature image  $U(z, p)$  is got in a form:

$$U(z, p) = -\frac{1}{p\sqrt{p} \cdot aC_p} \int_0^{\min\{z, \delta\}} q_0(z') \cdot sh \frac{(z-z')\sqrt{p}}{a} dz' + A_0 ch \frac{z\sqrt{p}}{a}.$$

Here  $A_0$  is defined with the use of boundary condition at the outlet target surface  $z = \Delta$ . In the ideal case of zero temperature maintained here, i.e.  $U(\Delta, p) = 0$ , the temperature image at  $z = 0$  is found as:

$$U(0, p) = \frac{q_{00}}{C_p p^2} \cdot \frac{\cosh \frac{\Delta \sqrt{p}}{a} - \cosh \frac{(\Delta - \delta) \sqrt{p}}{a}}{\cosh \frac{\Delta \sqrt{p}}{a}}.$$

In the limit  $p \rightarrow 0$  this defines the equilibrium temperature,  $T(z, \infty) = [pU(z, p)]_{p=0}$ , at inlet surface  $z = 0$  as:

$$T(0, \infty) = \frac{q_{00}}{C_p} \cdot \frac{\delta \cdot (2\Delta - \delta)}{2a^2}.$$

Here  $C_p$  stands for the heat capacity and  $a^2$  – for temperature conductivity coefficient.

With  $q_{00} \cong 65 \text{ kJ/g}$ , which corresponds to the heat flux of  $1 \text{ kJ/cm}^2/\text{s}$ ,  $\Delta = 0.5 \text{ mm}$  and  $\delta = 15 \mu\text{m}$  in molybdenum target  $T(0, \infty) = 36^\circ \text{C}$ .

Temperature dependence on time is described as:

$$T(0, t) = \frac{q_{00}}{a^2 C_p} \left[ \frac{(2\Delta - \delta) \cdot \delta}{2} - 2\Delta^2 \left( \frac{2}{\pi} \right)^3 \sum_{k=1}^{\infty} \frac{1}{(2k-1)^3} \cdot \sin \frac{(2k-1)\pi\delta}{2\Delta} \cdot \exp \left( - \frac{(2k-1)^2 \pi^2 a^2 t}{4\Delta^2} \right) \right].$$

The first term in the sum ( $k = 1$ ) forms more than 80% of the whole sum even at  $t = 0$ . Its characteristic time  $\tau_{\infty,1} = \frac{4\Delta^2}{\pi^2 a^2}$  defines in the main the temperature stabilization time  $\tau_{\infty} \cong \tau_{\infty,1}$ . The

effective rate of heating appears to be by a ratio  $\sim \frac{\pi^2 \delta}{4\Delta}$  less than its initial value  $\frac{\partial T(0, t)}{\partial t} \Big|_{t=0} = \frac{q_{00}}{C_p}$ ,

which maintains during a very short time  $\tau_0 \sim \frac{4\delta^2}{\pi^2 a^2}$  only. For  $\delta = 15 \mu\text{m}$  in molybdenum target this time is equal to  $\sim 1.7 \mu\text{s}$ , while the stabilization time with  $\Delta = 0.5 \text{ mm}$  is equal to  $\tau_{\infty} \cong 1.86 \text{ ms}$ .

Distribution of equilibrium temperature over target depth is found from solution of equation  $\frac{\partial^2 T}{\partial z^2} + \frac{q_0(z)}{C_p a^2} = 0$  with above defined boundary conditions. It has a form of Fourier series

$$T(z, \infty) = \sum_{n=1}^{\infty} T_n \cdot \cos \nu z, \text{ where } \nu = \frac{(2n-1)\pi}{2\Delta}, T_n = \frac{q_{0n}}{C_p a^2 \nu^2} \text{ and } q_{0n} = 2q_{00} \cdot \frac{\sin \nu \delta}{\nu \Delta}.$$

As a real approach to the heat evacuation scheme let's consider the cooling of target with the turbulent flow of liquid metal over the outlet target surface. The boundary condition here is determined through an achievable value of the specific heat transfer  $Q = \lambda_2 Nu \cdot (T - T_0) / l$ , defined with the heat conductivity of liquid  $\lambda_2$ , temperature difference between the target surface and liquid,  $T - T_0$ , characteristic size of the liquid metal stream  $l$  and the Nusselt coefficient  $Nu$ . With  $T_0$  put zero the boundary condition at  $z = \Delta$  is got in a form  $\lambda_1 \frac{\partial T}{\partial z} \Big|_{z=\Delta} = -\lambda_2 Nu \cdot \frac{T}{l}$ , where  $\lambda_1$  is the heat conductivity of target material.

Temperature image at inlet surface with this new condition at the outlet one gets a form:

$$U(0, p) = \frac{q_{00}}{C_\rho p^2} \cdot \frac{\cosh \frac{\Delta \sqrt{p}}{a} - \cosh \frac{(\Delta - \delta) \sqrt{p}}{a} + \frac{\lambda_1}{\lambda_2} \cdot \frac{l \sqrt{p}}{a Nu} \left[ \sinh \frac{\Delta \sqrt{p}}{a} - \sinh \frac{(\Delta - \delta) \sqrt{p}}{a} \right]}{\cosh \frac{\Delta \sqrt{p}}{a} + \frac{\lambda_1}{\lambda_2} \cdot \frac{l \sqrt{p}}{a Nu} \cdot \sinh \frac{\Delta \sqrt{p}}{a}}$$

This defines the equilibrium temperature  $T(z, \infty) = [pU(z, p)]_{p=0}$  as being equal to  $T(0, \infty) \cong \frac{q_{00} \delta}{C_\rho a^2} \cdot \left( \frac{2\Delta - \delta}{2} + \frac{l}{Nu} \cdot \frac{\lambda_1}{\lambda_2} \right)$  at  $z = 0$  and to  $T(\Delta, \infty) \cong \frac{q_{00} \delta}{C_\rho a^2} \cdot \frac{l}{Nu} \cdot \frac{\lambda_1}{\lambda_2}$  at  $z = \Delta$ .

For liquid metal, flowing through the channels, the Nusselt coefficient is found as  $Nu \cong 4.5 + 0.014 Pe^{0.8}$ , where  $Pe = \frac{u_0 l}{a^2}$ ,  $u_0$  - flow velocity and  $l$  - channel diameter. For target of the molybdenum, cooled with the liquid gallium, flowing through the channels of diameter  $l = 2$  mm with velocity  $v_0 = 10$  m/s, one gets  $Nu = 14.1$ . With  $q_{00} \cong 65$  kJ/g the equilibrium temperature at outlet surface  $T(\Delta, \infty)$  is equal to  $45^\circ C$ , while at the inlet one - to  $81^\circ C$ , more than two times higher as compared to the ideal case  $T(\Delta, t) \cong 0$ .

Temperature dependence on time is still described by means of expression:

$$T(0, t) = T(0, \infty) - \frac{q_{00}}{a^2 C_\rho} \cdot 2\Delta^2 \sum_{k=1}^{\infty} B_k \cdot \exp\left(-\frac{\phi_k^2 a^2 t}{\Delta^2}\right). \text{ However } \phi_k \text{ now are the roots of}$$

equation:  $\cos \phi - \frac{\lambda_1}{\lambda_2} \cdot \frac{l}{\Delta \cdot Nu} \cdot \phi \sin \phi = 0$ , i.e.  $\phi \cdot \operatorname{tg} \phi \cong 0.81$  for values of  $l$  and  $v_0$  accepted above. The first of roots, which defines in the main the characteristic time of temperature stabilization, is  $\phi_1 \cong 0.506 \cdot \frac{\pi}{2}$ , i.e. about two times less than in the ideal case. Time of temperature stabilization becomes equal to  $\tau_\infty \cong 7.2$  ms.

The equilibrium temperature distribution in target with new boundary condition still has a form of series  $T(x, y, z) = \sum_{m=1}^{\infty} T_m(x, y) \cos \mu_m z$  with  $\mu_m$  being the roots of equation  $\lambda_1 \mu \sin \mu \Delta = \frac{\lambda_2 Nu}{l} \cdot \cos \mu \Delta$ .

For a beam, moving about the target with velocity  $u_0$  in transverse direction  $x$ , for instance, the particle density distribution along this direction is to be taken into account, while in another one the beam still may be considered as homogeneous:  $T_m(x, y) \cong T_m(x)$ .

In the coordinate frame where the beam rests an equation for  $T_m(x)$  reads:

$$\frac{\partial^2 T_m}{\partial x^2} - \frac{u_0}{a^2} \frac{\partial T_m}{\partial x} - \mu_m^2 T_m + \frac{q_m(x)}{a^2 C_\rho} = 0.$$

Here  $q_m(x)$  are the coefficients of specific power expansion in a series  $q(x, z) = \sum_{m=1}^{\infty} q_m(x) \cos \mu_m z$  with above defined  $\mu_m$ . With supposition made about the specific power dependence on  $z$  one gets  $q_m(x) = q_0(x) \cdot \frac{4 \sin \mu_m \delta}{2 \mu_m \Delta + \sin 2 \mu_m \Delta}$ , where  $q_0(x)$  stands for specific power at the inlet target surface.

Solution for  $m$  - component of equilibrium temperature is got as:

$$T_m(x) = \frac{1}{a^2 C_\rho (D_1 - D_2)} \left[ \int_x^\infty q_m(x') \exp[D_1(x - x')] dx' + \int_{-\infty}^x q_m(x') \exp[D_2(x - x')] dx' \right],$$

with  $D_1, D_2$  being the roots of characteristic equation  $D^2 - \frac{u_0}{a} D - \mu_m^2 T_m = 0$ , i.e.

$$D_{1,2} = \frac{u_0}{2a^2} \pm \sqrt{\left(\frac{u_0}{2a^2}\right)^2 + \mu_m^2}.$$

Let  $q_0(x)$  be an infinite series of rectangles of height  $q_{00}$  and width  $\Delta x$ , distant from each other by  $X_0$  between the centers. Within the rectangle,  $-\frac{\Delta x}{2} \leq x \leq \frac{\Delta x}{2}$ , the solution has a form:

$$T_m(x) = \frac{q_{0m}}{a^2 C_\rho (D_1 - D_2)} \left\{ \frac{1}{D_1} \left[ 1 - e^{-D_1 \left(\frac{\Delta x}{2} - x\right)} + 2 \sinh \frac{D_1 \Delta x}{2} \cdot \frac{e^{-D_1 (X_0 - x)}}{1 - e^{-D_1 X_0}} \right] - \frac{1}{D_2} \left[ 1 - e^{-D_2 \left(\frac{\Delta x}{2} + x\right)} - 2 \sinh \frac{D_2 \Delta x}{2} \cdot \frac{e^{D_2 (X_0 + x)}}{1 - e^{D_2 X_0}} \right] \right\}$$

and between them,  $\frac{\Delta x}{2} \leq x \leq X_0 - \frac{\Delta x}{2}$ :

$$T_m(x) = \frac{2q_{0m}}{a^2 C_\rho (D_1 - D_2)} \left\{ \frac{1}{D_1} \sinh \frac{D_1 \Delta x}{2} \cdot \frac{e^{-D_1 (X_0 - x)}}{1 - e^{-D_1 X_0}} + \frac{1}{D_2} \sinh \frac{D_2 \Delta x}{2} \cdot \frac{e^{D_2 x}}{1 - e^{D_2 X_0}} \right\}.$$

In a limit of extremely large velocity  $u_0$  both these expressions transform into  $T_m(x) \cong \frac{q_{0m}}{a^2 C_\rho \mu_m^2} \frac{\Delta x}{X_0}$ , which corresponds to the homogeneously distributed power deposition of specific value, decreased as compared to  $q_{00}$  in proportionality to the ratio  $\frac{\Delta x}{X_0}$ . Condition for such

a transformation is the  $\mu_m$  smallness as compared to  $\frac{u_0}{a^2}$ :  $\mu_m^2 \ll \left(\frac{u_0}{2a^2}\right)^2$ . In the case of

molybdenum target cooled with gallium, for the first root of equation  $\mu \Delta \cdot \tan \mu \Delta \cong \frac{Nu \cdot \Delta}{l} \cdot \frac{\lambda_2}{\lambda_1}$ ,

$\mu_1 \Delta \cong 0.506 \cdot \frac{\pi}{2}$ , this is fulfilled at  $u_0 > 20$  cm/s.

When the water is used for target cooling instead of the liquid gallium by the same geometric parameters and flow velocity, the equation for  $\mu_m$  definition reads  $\mu \Delta \cdot \tan \mu \Delta \cong 0.172$ . Time of temperature stabilization, defined with the first root  $\mu_1 \Delta \cong 0.403$ , is equal to  $\sim 28$  msec. Equilibrium temperature at inlet target surface is by  $\sim 6.8$  times higher than in the ideal case, and three times higher as compared to the liquid gallium cooling.